PCT

WORLD INTELLECTUAL PROPERTY ORGANIZATION International Bureau



INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification ⁶ : A61K 9/14	A1	 (11) International Publication Number: WO 95/31974 (43) International Publication Date: 30 November 1995 (30.11.95)
(22) International Application Number: PCT/US (22) International Filing Date: 12 May 1995 (30) Priority Data: 08/249,781 25 May 1994 (25.05.94) (71) Applicant (for all designated States except US): E. KODAK COMPANY [US/US]; 343 State Street, I. NY 14650 (US). (72) Inventors; and (75) Inventors/Applicants (for US only): CZEKAI, I. [US/US]; 133 Amann Road, Honeoye Falls, N. (US). SEAMAN, Larry, P. [US/US]; 7886 Unior Road, Mount Morris, NY 14510 (US). (74) Agent: ROSENSTEIN, Arthur, H.; 343 State Street, I. NY 14650-2201 (US).	LASTMA Rocheste David, ANY 1447 on Corne	EE, FI, GE, HU, JP, KE, KG, KP, KR, KZ, LK, LR, LT, LV, MD, MG, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SG, SI, SK, TJ, TT, UA, US, UZ, VN, European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG). Published With international search report. Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments. A.

(57) Abstract

A method of preparing submicron particles of a therapeutic or diagnostic agent which comprises grinding the agent in the presence of grinding media having a mean particle size of less than about 75 microns. In a preferred embodiment, the grinding media is a polymeric resin. The method provides extremely fine particles, e.g., less than 100 nanometers in size, free of unacceptable contamination.

FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AT	Austria	GB	United Kingdom	MR	Mauritania
ΑŪ	Australia	GE	Georgia	MW	Malawi
BB	Barbados	GN	Guinea	NE	Niger
BE	Belgium	GR	Greece	NL	Netherlands
BF	Burkina Faso	HU	Hungary	NO	Norway
BG	Bulgaria	IE	Ireland	NZ	New Zealand
BJ	Benin	IT	Itały	PL	Poland
BR	Brazil	JP	Japan	PT	Portugal
BY	Belarus	KE	Kenya	RO	Romania
CA	Canada	KG	Kyrgystan	RU	Russian Federation
CF	Central African Republic	KP	Democratic People's Republic	SD	Sudan
CG	Congo		of Korea	SE	Sweden
CH	Switzerland	KR	Republic of Korea	SI	Slovenia
CI	Côte d'Ivoire	KZ	Kazakhstan	SK	Slovakia
CM	Cameroon	LI	Liechtenstein	SN	Senegal
CN	China	LK	Sri Lanka	TD	Chad
CS	Czechoslovakia	LU	Luxembourg	TG	Togo
CZ	Czech Republic	LV	Latvia	TJ	Tajikistan
DE	Germany	MC	Monaco	TT	Trinidad and Tobago
DK	Denmark	MD	Republic of Moldova	UA	Ukraine
ES	Spain	MG	Madagascar	US	United States of America
FI	Finland	ML	Mali	UZ	Uzbekistan
FR	France	MN	Mongolia	VN	Viet Nam
GA	Gabon				

WO 95/31974 PCT/US95/06035

METHOD OF GRINDING PHARMACEUTICAL SUBSTANCES

BACKGROUND OF THE INVENTION

5 Various grinding media, such as stainless steel, zirconium silicate, zirconium oxide, glass, and the like, typically in the form of spherical beads, are commonly used in various mills, including media mills, for grinding materials. Heretofore, efforts have been made to control the size and size 10 range of drug particles in pharmaceutical compositions by a variety of methods, including various milling techniques, such as airjet milling and wet milling. However, there tends to be a bias in the pharmaceutical arts against milling techniques, particularly wet milling, due to concerns associated with 15 contamination. For example, in the preparation of pharmaceuticals for oral and parenteral applications, it is desirable to have total contamination, e.g., of heavy metals, below about 10 parts per million. The need to control and minimize contamination is particularly critical in the milling 20 of parenteral products due to potential safety issues associated with injection of contaminants.

Liversidge et al, U.S. Patent No. 5,145,684, and
European Patent Application 498,492, describe dispersible
particles consisting of a drug substance or an x-ray contrast
25 agent having a surface modifier adsorbed on the surface thereof
in an amount sufficient to maintain an effective average
particle size of less than about 400 nm. The particles are
prepared by dispersing a drug substance or imaging agent in a
liquid dispersion medium and wet grinding in the presence of
30 rigid grinding media.

Bruno et al, commonly-owned U.S. Patent Application Serial No. 07/981,639 filed November 25, 1992 entitled Method for Grinding Pharmaceutical Substances discloses polymeric grinding media for fine grinding pharmaceutical compositions. Bruno et al disclose that the media can be in the size range of 0.1-3 mm (100-3000 microns). The media specifically exemplified in the working examples have a mean particle size in the range of 0.3-0.6 mm (300-600 microns).

PCT/US95/06035

-2-

In practicing the methods described by Liversidge et al and Bruno et al, dispersions comprising therapeutic and diagnostic agents having particle sizes as small as about 100 nm have been obtained on some occasions. However, for many applications, e.g., when further increased bioavailability and/or targeting to a specific tissue site is desired, it would be highly advantageous to produce dispersions free of unacceptable contamination having a particle size of less than 100 nm.

10

WO 95/31974

SUMMARY OF THE INVENTION

We have discovered that extremely fine particles, e.g., of a size less than 100 nanometers, of therapeutic and diagnostic agents free of unacceptable contamination can be prepared by milling in the presence of grinding media having a mean particle size of less than about 75 microns.

More specifically, in accordance with this invention, there is provided a method of preparing particles of a

20 therapeutic or diagnostic agent which comprises grinding the agent in the presence of grinding media having a mean particle size of less than about 75 microns.

It is a particularly advantageous feature of this invention that there is provided a method of preparing extremely fine particles of therapeutic and diagnostic agents free of unacceptable contamination and/or discoloration.

Still another advantageous feature of this invention is that there is provided a method of fine grinding therapeutic and diagnostic agents, which method generates less heat and reduces potential heat-related problems such as chemical instability and contamination.

It is another advantageous feature of this invention that a method of fine grinding drugs and imaging agents is provided enabling improved pH control.

Other advantageous features will become apparent upon reference to the following Description of Preferred Embodiments.

DESCRIPTION OF PREFERRED EMBODIMENTS

This invention is based partly on the unexpected discovery that therapeutic and diagnostic agents can be

5 prepared in extremely fine particles free of unacceptable contamination by grinding in the presence of extremely fine grinding media. While this invention is described herein in connection with its preferred utilities, i.e., with respect to therapeutic agents for use in pharmaceutical compositions and diagnostic agents for use in medical diagnostic compositions, it is also believed to be useful in other applications, such as the grinding of particles for cosmetic compositions, where extremely fine particle size is desired and contamination can be a concern.

In the method of this invention, a therapeutic or diagnostic agent is prepared in the form of submicron particles by grinding the agent in the presence of a grinding media having a mean particle size of less than about 75 microns.

In a preferred embodiment, the grinding media can
comprise particles, preferably substantially spherical in
shape, e.g., beads, of a polymeric resin. However, grinding
media in the form of other non-spherical shapes are expected to
be useful in the practice of this invention.

In general, polymeric resins suitable for use herein are chemically and physically inert, substantially free of metals, solvent and monomers, and of sufficient hardness and friability to enable them to avoid being chipped or crushed during grinding. Suitable polymeric resins include crosslinked polystyrenes, such as polystyrene crosslinked with

- divinylbenzene, styrene copolymers, polyacrylates such as polymethyl methylcrylate, polycarbonates, polyacetals, such as Delrin™, vinyl chloride polymers and copolymers, polyurethanes, polyamides, poly(tetrafluoroethylenes), e.g., Teflon™, and other fluoropolymers, high density polyethylenes,
- 35 polypropylenes, cellulose ethers and esters such as cellulose acetate, polyhydroxymethacrylate, polyhydroxyethyl acrylate, silicone containing polymers such as polysiloxanes and the like. The polymer can be biodegradable. Exemplary

WO 95/31974 PCT/US95/06035

-4-

biodegradable polymers include poly(lactides), poly(glycolide) copolymers of lactides and glycolide, polyanhydrides, poly(hydroxyethyl methacrylate), poly(imino carbonates), poly(N-acylhydroxyproline)esters, poly(N-palmitoyl hydroxyproline) esters, ethylene-vinyl acetate copolymers, poly(orthoesters), poly(caprolactones), and poly(phosphazenes). In the case of biodegradable polymers, contamination from the media itself advantageously can metabolize in vivo into biologically acceptable products which can be eliminated from the body.

The polymeric resin can have a density from 0.8 to $3.0~\rm g/cm^3$. Higher density resins are preferred inasmuch as it is believed that these provide more efficient particle size reduction.

Furthermore, Applicants believe that the invention can be practiced in conjunction with various inorganic grinding media prepared in the appropriate particle size. Such media include zirconium oxide, such as 95% ZrO stabilized with magnesia, zirconium silicate, glass, stainless steel, titania, alumina, and 95% ZrO stabilized with yttrium.

The media can range in size up to about 100 microns. For fine grinding, the particles preferably are less than about 75 microns, more preferably, less than about 50 microns, and, most preferably, less than about 25 microns, in size.

25 Excellent particle size reduction has been achieved with media having a particle size of about 5 microns.

The milling process can be a dry process, e.g., a dry roller milling process, or a wet process, i.e., wet-grinding. In preferred embodiments, this invention is practiced in 30 accordance with the wet-grinding process described in U.S. Patent No. 5,145,684 and European Patent Application 498,482. Thus, the wet grinding process can be practiced in conjunction with a liquid dispersion medium and surface modifier such as described in these publications. Useful liquid dispersion 35 media include water, aqueous salt solutions, ethanol, butanol, hexane, glycol and the like. The surface modifier can be selected from known organic and inorganic pharmaceutical excipients such as described in U.S. Patent No. 5,145,684 and

can be present in an amount of 0.1-90%, preferably 1-80% by weight based on the total weight of the dry particle.

In preferred embodiments, the therapeutic or diagnostic agent can be prepared in submicron or

5 nanoparticulate particle size, e.g., less than about 500 nm.
Applicants have demonstrated that particles can be prepared having an average particle size of less than about 300 nm. In certain embodiments, particles having an average particle size of less than 100 nm have been prepared in accordance with the present invention. It was particularly surprising and unexpected that such fine particles could be prepared free of unacceptable contamination.

Grinding can take place in any suitable grinding mill. Suitable mills include an airjet mill, a roller mill, a ball mill, an attritor mill, a vibratory mill, a planetary mill, a sand mill and a bead mill. A high energy media mill is preferred especially when the grinding media is a polymeric resin. The mill can contain a rotating shaft. This invention can also be practiced in conjunction with high speed dispersers such as a Cowles disperser, rotor-stator mixers, or other conventional mixers which can deliver high fluid velocity and high shear.

The preferred proportions of the grinding media, the therapeutic and/or diagnostic agent, the optional liquid
25 dispersion medium, and surface modifier present in the grinding vessel can vary within wide limits and depends, for example, upon the particular drug substance or imaging agent selected, the size and density of the grinding media, the type of mill selected, etc. The process can be carried out in a continuous,
30 batch or semi-batch mode. In high energy media mills, it can be desirable to fill 70-90% of the volume of the grinding chamber with grinding media. On the other hand, in roller mills, it frequently is desirable to leave the grinding vessel up to half filled with air, the remaining volume comprising the grinding media and the liquid dispersion media, if present. This permits a cascading effect within the vessel on the rollers which permits efficient grinding. However, when

PCT/US95/06035

WO 95/31974

foaming is a problem during wet grinding, the vessel can be completely filled with the liquid dispersion medium.

-6-

The attrition time can vary widely and depends primarily upon the particular therapeutic or diagnostic agent,

5 mechanical means and residence conditions selected, the initial and desired final particle size and so forth. For roller mills, processing times from several days to weeks may be required. On the other hand, residence times of less than about 8 hours are generally required using high energy

10 dispersers and/or media mills.

After attrition is completed, the grinding media is separated from the milled particulate product (in either a dry or liquid dispersion form) using conventional separation techniques, such as by filtration, sieving through a mesh screen, and the like.

The invention can be practiced with a wide variety of therapeutic and diagnostic agents. In the case of dry milling, the drug substances and imaging agents must be capable of being formed into solid particles. In the case of wet milling, the drug substances and imaging agents must be poorly soluble and dispersible in at least one liquid medium. By "poorly soluble", it is meant that the therapeutic or diagnostic agent has a solubility in the liquid dispersion medium, e.g., water, of less than about 10 mg/ml, and preferably of less than about 1 mg/ml. The preferred liquid dispersion medium is water. Additionally, the invention can be practiced with other liquid media. The therapeutic and diagnostic agents preferably are organic, crystalline materials.

Suitable therapeutic agents and classes of

therapeutic agents are described in U.S. Patent No. 5,145,684
and include Danazol, 5α, 17α,-1'-(methylsulfonyl)-1'H-pregn-20yno[3,2-c]-pyrazol-17-ol, camptothecin, piposulfam, piposulfan,
naproxen and phenytoin. Other suitable drug substances include
the NSAIDs described in PCT International Application

PCT/US93/05082 published December 23, 1993 and the anticancer
agents described in European Patent Application 577,215

published January 5, 1993.

Suitable diagnostic agents include derivatives of iodinated aromatic acids such as ethyl-3,5-bisacetoamido-2,4,6-triiodobenzoate (WIN 8883), ethyl(3,5-bis(acetylamino)-2,4,6-triiodobenzoyloxy) acetate (WIN 12901), ethyl-2-

- (bis(acetylamino)-2,4,6-triiodobenzoyloxy)butyrate (WIN 16318), 6-ethoxy-6-oxohexyl-3,5-bis(acetylamino)-2,4,6-triiodobenzoate (WIN 67722). Other suitable imaging agents are described in U.S. Patent No. 5,260,478, U.S. Patent No. 5,264,610 and European Patent Application 498,482.
- The following examples further illustrate the invention.

Example 1 Effect of Media Size on Danazol Dispersion

- A Danazol premix dispersion was prepared by combining 30% w/w Danazol (2-10 µm mean size powder), 10% polyvinyl pyrrolidone (PVP) having an average molecular weight of 15,000, and water. Polystyrene beads crosslinked with divinyl benzene (20% styrene, 80% divinylbenzene) were prepared by conventional
- polymerization techniques with mean diameters of 5, 25, 50, 200 and 450 microns. The 450 µm beads were added to the grinding chamber (300 ml, grade 316 stainless steel) of a Dyno-Mill (Model KDL-Special, manufactured by Chicago Boiler). A control dispersion was prepared by milling the premix dispersion for
- 25 120 minutes residence time. After milling, the control dispersion was diluted with water to a final concentration of 5% Danazol, 1.5% PVP and was further milled in a high energy attrition mill using the various sized polystyrene media for 60 minutes (recirculation time). The dispersion was separated
- 30 from the media by 5 μm filtration, and the particle size measured by capillary hydrodynamic fractionation (CHDF) was as follows:

PCT/US95/06035

WO 95/31974

-8-

Weight	Average
--------	---------

	Media Size (microns)	Danazol Particle Size (nm)
	Control	149
5	450	105
	200	86
	50	80
	25 ·	92 (possible flocculation)

10 These results indicate that particles having a mean size of less than 100 nm can be prepared in accordance with this invention.

Example 2 Grinding with 5 Micron Size Media

In a subsequent experiment, the 5 micron polystyrene media described above was used under grinding conditions similar to those described above. The resulting dispersion particle size was 105 nm. It was entirely unexpected that excellent communition was achieved with such fine microscopic polymeric media. In aqueous solution, the 5 micron media appears as a milky solution to the unaided eye.

Example 3 Continuous Milling Process Using Fine Polymeric Media in a 0.3 Liter DynoMill

A premix dispersion was formed by combining micronized Danazol powder (2-10μm mean size) with an aqueous PVP (avg. MW = 15,000) solution at a ratio of 5.0% Danazol, 1.5% PVP and 93.5% water. 292 grams of this premix dispersion was combined with 379.6 grams of polystyrene crosslinked with divinyl benzene (20:80 w/w) milling media, nominal 50 micron size. This combined mixture was recirculated through a 0.3 liter DynoMill at 3200 rpm (100cm³/min) for 60 minutes (residence time). After milling, the media was separated using a 10 μm filter. After milling the particle size was measured by CHDF. The particle size distribution showed a weight average particle size of 35 nm.

Example 4 Continuous Milling Process Using Fine Polymeric Media in a 0.6 Liter DynoMill

A premix dispersion was formed by combining micronized Danazol powder (2-10 μm mean size) with an aqueous 5 PVP (avg. MW = 15,000) solution at a ratio of 5.0% Danazol, 1.5% PVP and 93.5% water. 2768 grams of this premix dispersion was combined with 3324 grams of polystyrene crosslinked with divinyl benzene (20:80 w/w) recirculated through a 0.6 liter DynoMill at 3200 rpm (100 cm3/min) for 60 minutes residence time. After milling, the media was separated using a 10 μm filter. The particle size of this batch was not measured but microscopic examination indicated that the mean size was likely below 100 nm.

The invention has been described in detail with

15 particular reference to certain preferred embodiments thereof,
but it will be understood that variations and modifications can
be effected within the spirit and scope of the invention.

WO 95/31974

-10-

Claims:

- A method of preparing submicron particles of a therapeutic agent comprising grinding said agent in the presence of rigid
 grinding media having a mean particle size of less than about
 microns.
 - 2. The method of claim 1 wherein said media is a polymeric resin.

10

- 3. The method of claim 1 wherein said media have a mean particle size of less than 50 microns.
- 4. The method of claim 1 wherein said grinding media have an 15 average size of about 5 microns.
 - 5. The method of claim 2 wherein said polymer is polystyrene crosslinked with divinyl benzene.
- 20 6. The method of claim 2 wherein said polymer is polymethylmethacrylate.
 - 7. The method of claim 1 wherein said method is a wet grinding process.

- 8. The method of claim 1 wherein said grinding takes place in a high shear disperser, a rotor-stator mixer or a mill selected from an airjet mill, a roller mill, a ball mill, an attritor mill, a vibratory mill, a planetary mill, a sand mill, and a
- 30 bead mill.
 - 9. The method of claim 1 wherein said therapeutic agent is Danazol.
- 35 10. A method of preparing submicron particles of a diagnostic agent comprising grinding said agent in the presence of a rigid grinding media having a mean particle size of less than about 75 microns.

10

- 11. The method of claim 10 wherein said media is a polymeric resin.
- 5 12. The method of claim 10 wherein said media have a mean particle size of less than 50 microns.
 - 13. The method of claim 10 wherein said grinding media have an average size of about 5 microns.
 - 14. The method of claim 11 wherein said polymer is polystyrene crosslinked with divinyl benzene.
- 15. The method of claim 11 wherein said polymer is polymethylmethacrylate.
 - 16. The method of claim 10 wherein said method is a wet grinding process.
- 20 17. The method of claim 10 wherein said grinding takes place in a high shear disperser, a rotor-stator mixer or a mill selected from an airjet mill, a roller mill, a ball mill, an attritor mill, a vibratory mill, a planetary mill, a sand mill, and a bead mill.
 - 18. The method of claim 10 wherein said diagnostic agent is selected from the group consisting of WIN 8883, WIN 12901, WIN 16318, and WIN 67722.

Interr hal Application No

PCT/US 95/06035 A. CLASSIFICATION OF SUBJECT MATTER IPC 6 A61K9/14 According to International Patent Classification (IPC) or to both national classification and IPC Minimum documentation searched (classification system followed by classification symbols) IPC 6 A61K Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched Electronic data base consulted during the international search (name of data base and, where practical, search terms used) C. DOCUMENTS CONSIDERED TO BE RELEVANT Relevant to claim No. Citation of document, with indication, where appropriate, of the relevant passages 1-4,6,8, X DATABASE WPI 10-13, Section Ch, Week 8821 Derwent Publications Ltd., London, GB; 15,17 Class A96, AN 88-1444226 & JP,A,63 086 760 (PENTEL KK) , 18 April 1988 see abstract & PATENT ABSTRACTS OF JAPAN X 1-4,6,8, vol. 12 no. 316,26 August 1988 10-13, & JP,A,63 086760 (PENTEL KK) 18 April 15,17 see abstract X EP,A,O 371 431 (VECTORPHARMA INTERNATIONAL 1-3, SPA) 6 June 1990 10-12 see page 5; examples 5,6 -/--| X | Further documents are listed in the continuation of box C. Patent family members are listed in annex. * Special categories of cited documents: "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the "A" document defining the general state of the art which is not considered to be of particular relevance invention earlier document but published on or after the international "X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to filing date document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) involve an inventive step when the document is taken alone "Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such docu-"O" document referring to an oral disclosure, use, exhibition or ments, such combination being obvious to a person skilled in the art. other means document published prior to the international filing date but later than the priority date claimed "&" document member of the same patent family Date of the actual completion of the international search Date of mailing of the international search report 1 0. 10. 95 3 October 1995 Name and mailing address of the ISA Authorized officer European Patent Office, P.B. 5818 Patentlaan 2 NL - 2280 HV Rijswijk Tel. (+31-70) 340-2040, Tx. 31 651 epo ni, Boulois, D Fax: (+31-70) 340-3016

Form PCT/ISA/210 (second sheet) (July 1992)

INTERNATIONAL SEARCH REPORT

Interr val Application No
PCT/US 95/06035

0.15		PCT/US 95/06035	
C.(Continua Category	ntion) DOCUMENTS CONSIDERED TO BE RELEVANT	Ind.	
Caugory	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.	
A	EP,A,O 499 299 (STERLING WINTHROP INC.) 19 August 1992 cited in the application see page 6 - page 7; example 1	1-18	
	DE,A,37 17 818 (ASAHI KOGAKU KOGYO KK) 3 December 1987 see column 5, line 25 - line 43	1-18	
		-	

INTERNATIONAL SEARCH REPORT

information on patent family members

Enterr sal Application No
PCT/US 95/06035

Patent document cited in search report	Publication date	Patent family member(s)		Publication date
EP-A-371431	06-06-90	AT-T- CA-A- DE-D- IL-A- JP-A- SU-A- US-A- US-A-	123940 2004064 68923157 92454 2184621 1837868 5449521 5354560	15-07-95 28-05-90 27-07-95 24-06-94 19-07-90 30-08-93 12-09-95 11-10-94
EP-A-499299	19-08-92	US-A- AU-B- AU-B- AU-B- AU-B- EP-A- JP-A- JP-A-	5145684 642066 1014592 654836 1014792 0498482 4317053 4295420	08-09-92 07-10-93 30-07-92 24-11-94 30-07-92 12-08-92 09-11-92 20-10-92
 DE-A-3717818	03-12-87	US-A- US-A- JP-B- JP-A- FR-A- GB-A,B US-A-	5399363 5318767 2005087 62281953 2607008 2192389 5064436	21-03-95 07-06-94 31-01-90 07-12-87 27-05-88 13-01-88 12-11-91